Power System Analysis

Chapter 11 Power System Operation

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Outline

- 1. Overview
- 2. Unit commitment
- 3. Optimal dispatch
- 4. Frequency control
- 5. System security

Overview Central challenge

Balance supply & demand second-by-second

- While satisfying operational constraints, e.g. injection/voltage/line limits
- Unlike usual commodities, electricity cannot (yet) be stored in large quantity

Overview Traditional approach

Bulk generators generate 80% of electricity in US (2020)

• Fossil (gas, coal): 60%, nuclear: 20%

They are fully dispatchable and centrally controlled

• ISO determines in advance how much each generates when & where

They mostly determine dynamics and stability of entire network

• System frequency, voltages, prices

Overview Traditional approach

Challenges

- Large startup/shutdown time and cost
- Uncertainty in future demand (depends mostly on weather)
- Contingency events such as generator/transmission outages

Elaborate electricity markets and hierarchical control

- Schedule generators and determine wholesale prices
- Day-ahead (12-36 hrs in advance): unit commitment
- Real-time (5-15 mins in advance): economic dispatch
- Ancillary services (secs hours): frequency control, reserves

Overview Future challenges

Sharply increased uncertainty makes balancing more difficult

- Renewable sources such as wind and solar
- Random large frequent fluctuations in net load, e.g., Duck Curve due to PV
- Contingency events such as generator/transmission outages
- Response: real-time feedback control, better monitoring & forecast, stochastic OPF

Low-inertia system

- Bulk generators have large inertia that is bedrock of stability
- They will be replaced by inverter-based resources with low or zero inertia, e.g., PV
- Response: dynamics and stability need to be re-thought

Indispatchable renewable generation resources

• *Response*: More active dynamic feedback control of flexible loads to match fluctuating supply

Overview Optimal power flow

Unit commitment and economic dispatch can be formulated as OPF

- OPF underlies many (other) power system applications
- State estimation, stability and security analysis, volt/var control, demand response

Constrained optimization

 $\min_{u,x} c(u,x) \quad \text{s.t.} \quad f(u,x) = 0, \ g(u,x) \le 0$

- Optimization vars: control *u*, network state *x*
- Cost function: c(u, x)
- Constraint functions: f(u, x), g(u, x)
- They depend on the application under study

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Unit commitment

Solved by ISO in day-ahead market 12-36 hrs in advance

- Determine which generators will be on (commitment) and their output levels (dispatch)
- For each hour (or half hour) over 24-hour period
- Commitment decisions are binding
- Dispatch decisions may be binding or advisory

Two-stage optimization

• Determine commitment, based on assumption that dispatch will be optimized

Model

- Network: graph $G = (\overline{N}, E)$
- Time horizon: $T := \{1, 2, ..., T\}$, e.g., t = 1 hour, T = 24

Optimization vars

- Control:
 - Commitment: on/off status $\kappa(t) := \left(\kappa_j(t), j \in \overline{N}\right), \ \kappa_j(t) \in \{0,1\}$
 - Dispatch: real & reactive power injections $u(t) := (u_j(t), j \in \overline{N})$
- Network state:
 - Voltages $V(t) := (V_j(t), j \in \overline{N})$

• Line flows
$$S(t) := \left(S_{jk}(t), S_{kj}(t), (j,k) \in E\right)$$

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Capacity limits: injection is bounded if it is turned on

 $\underline{u}_{j}(t)\kappa_{j}(t) \leq u_{j}(t) \leq \overline{u}_{j}(t)\kappa_{j}(t)$

Startup and shutdown incur costs regardless of injection level

$$d_{jt}(\kappa_j(t-1),\kappa_j(t)) = \begin{cases} \text{startup cost} & \text{if } \kappa_j(t) - \kappa_j(t-1) = 1\\ \text{shutdown cost} & \text{if } \kappa_j(t) - \kappa_j(t-1) = -1\\ 0 & \text{if } \kappa_j(t) - \kappa_j(t-1) = 0 \end{cases}$$

UC problems in practice includes other features

• Once turned on/off, bulk generator stays in same state for minimum period

Two-stage optimization

$$\min_{\kappa \in \{0,1\}^{(N+1)T}} \sum_{t} \sum_{j} d_{jt} \left(\kappa_{j}(t-1), \kappa_{j}(t) \right) + c^{*}(\kappa)$$

where $c^*(\kappa)$ is optimal dispatch cost over entire horizon *T*:

$$c^{*}(\kappa) := \min_{(u,x)} \sum_{t} c_{t}(u(t), x(t); \kappa(t))$$

s.t. $f_{t}(u(t), x(t); \kappa(t)) = 0, g_{t}(u(t), x(t); \kappa(t)) \le 0, t \in T$
 $\tilde{f}(u, x) = 0, \ \tilde{g}(u, x) \le 0$

• Each time *t* constraint includes injection limits

• $\tilde{f}(u, x) = 0$, $\tilde{g}(u, x) \le 0$ can include ramp rate limits

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UC in practice

- Binary variable makes UC computationally difficult for large networks
- Typically use linear model, e.g., DC power flow, and solve mixed integer linear program

Serious effort underway in R&D community to scale UC solution with AC model

• e.g., ARPA-E Grid Optimization Competition Challenge 2

Outline

- 1. Overview
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3. Optimal dispatch

- OPF formulation
- Imbalance and error model
- 4. Frequency control
- 5. System security

Optimal dispatch

Solved by ISO in real-time market every 5-15 mins

- Determine injection levels of those units that are online
- Adjustment to dispatch from day-ahead market (unit commitment)

Optimal dispatch Problem formulation

Model

• Network: graph $G = (\overline{N}, E)$

Optimization vars

- Control:
 - Dispatch: real & reactive power injections $u := (u_j, j \in \overline{N})$
- Network state:
 - Voltages $V := (V_j, j \in \overline{N})$
 - Line flows $S := \left(S_{jk}, S_{kj}, (j,k) \in E\right)$

Optimal dispatch Problem formulation

Parameters

• Uncontrollable injections $\sigma := \left(\sigma_{j}, j \in \overline{N}\right)$

Generation cost is quadratic in real power

$$c(u, x) = \sum_{\text{generators } j} \left(a_j \left(\operatorname{Re}(u_j) \right)^2 + b_j \operatorname{Re}(u_j) \right)$$

Optimal dispatch Constraints

Power flow equations: S = S(V)

• Complex form:
$$S_{jk}(V) = (y_{jk}^s)^H (|V_j|^2 - V_j V_k^H) + (y_{jk}^m)^H |V_j|^2$$

• Polar form:

$$P_{jk}(V) = \left(g_{jk}^{s} + g_{jk}^{m}\right) |V_{j}|^{2} - |V_{j}| |V_{j}| \left(g_{jk}^{s} \cos(\theta_{j} - \theta_{k}) - b_{jk}^{s} \sin(\theta_{j} - \theta_{k})\right)$$
$$Q_{jk}(V) = \left(b_{jk}^{s} + b_{jk}^{m}\right) |V_{j}|^{2} - |V_{j}| |V_{k}| \left(b_{jk}^{s} \cos(\theta_{j} - \theta_{k}) + g_{jk}^{s} \sin(\theta_{j} - \theta_{k})\right)$$

Power balance: $u_j + \sigma_j = \sum_{k:j \sim k} S_{jk}(V)$

Optimal dispatch Constraints

Optimal dispatch

$$\min_{u,x} \quad c(u,x)$$
s.t.
$$u_j + \sigma_j = \sum_{k:j \sim k} S_{jk}(V)$$

$$\underline{u}_j \leq u_j \leq \overline{u}_j$$

$$\underline{v}_j \leq |V_j|^2 \leq \overline{v}_j$$

$$|S_{jk}(V)| \leq \overline{S}_{jk}, \quad |S_{kj}(V)| \leq \overline{S}_{kj}$$

 $u^{\mathrm{opt}}(\sigma)$: optimal dispatch driven by σ

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Optimal dispatch

Interpretation

- ISO dispatches u_i^{opt} to unit *j* as generation setpoint (needs incentive compatibility)
- Resulting network state x^{opt} satisfies operational constraints

Economic dispatch in practice

- Real-time market use linear approximation, e.g., DC power flow, instead of AC (nonlinear) power flow equations
- ISO solves linear program for dispatch and wholesale prices
- AC power flow equations are used to verify that operational constraints are satisfied if dispatched
- If not, DC OPF is modified and procedure repeated

Optimal dispatch Imbalance

In theory, power is balanced at all points of network, since (u^{opt}, x^{opt}) satisfies

$$u_j + \sigma_j = \sum_{k:j \sim k} S_{jk}(V)$$

Imbalance, however, arises due to

- Random error $\Delta_1(\xi, t)$
- Discretization error $\Delta_2(t)$
- Prediction error $\Delta_3(\xi, t)$

Optimal dispatch Error model

Uncontrollable injections $\sigma := (\sigma(t), t \in \mathbb{R}_+)$: continuous-time stochastic process

• Mean process $m(t) := E\sigma(t)$

 $u\left(\sigma(\xi,t)\right)$: actual injections that can maintain power balance over network Imbalance:

$$\Delta u(\xi, t) := u\left(\sigma(\xi, t)\right) - u^{\mathsf{opt}}\left(\hat{m}(n)\right), \quad t \in [n\delta, (n+1)\delta), \ n = 0, 1, \dots$$

	actual	dispatch on	
	injection	<i>n</i> th control	
	at time t	interval	
•	$u\left(\sigma(\xi,t)\right)$: random, continuous		

• $u^{\text{opt}}(\hat{m}(n))$: fixed for *n*th interval, based on estimate $\hat{m}(n)$ of σ

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Optimal dispatch Error model

Random error $\Delta_1(\xi, t) := u(\sigma(\xi, t)) - u^{\text{opt}}(m(t))$

• Dispatch driven by mean process, at all (continuous) time t

Discretization error $\Delta_2(t) := u^{\text{opt}}(m(t)) - u^{\text{opt}}(\bar{m}(n)), t \in [n\delta, (n+1)\delta)$ Dispatch driven by time-average over *n*th interval $\bar{m}(n) := \frac{1}{\delta} \int_{n\delta}^{(n+1)\delta} m(t) dt$

Prediction error $\Delta_3(\xi, t) := u^{\text{opt}}(\bar{m}(n)) - u^{\text{opt}}(\hat{m}(n)), t \in [n\delta, (n+1)\delta)$

- Dispatch driven by estimate $\hat{m}(n)$ of $\bar{m}(n)$ before beginning of *n*th interval
- $\hat{m}(n)$ generally depends on ξ and is random, e.g., avg injection in n-1 st interval

$$\hat{m}(\xi, n) := \frac{1}{\delta} \int_{(n-1)\delta}^{n\delta} \sigma(\xi, t) dt$$

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Optimal dispatch Error model

Imbalance:

$$\Delta u(\xi, t) = \Delta_1(\xi, t) + \Delta_2(t) + \Delta_3(\xi, t)$$

- Random error $\Delta_1(\xi, t)$: tends to have zero mean
- Discretization error $\Delta_2(t)$: time avg over control interval tends to be small
- Prediction error $\Delta_3(\xi, t)$: tends to be small if $\sigma(t)$ is slow-varying

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- 4. Frequency control
 - Model and assumptions
 - Primary frequency control
 - Secondary frequency control
- 5. System security

Power delivered by thermal generator is determined by mechanical output of turbine

- Mechanical output of turbine controlled by opening or closing of valves that regulate steam or water flow
- If load increases, valves will be opened wider to generate more power to balance

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Power imbalance \implies frequency deviates from nominal

- Excess supply: rotating machines speed up \Rightarrow frequency rises
- Shortage: rotating machines slow down \Rightarrow frequency drops
- If power is not re-imbalanced, frequency excursion will continue and may disconnect generators to protect them from damage
- Can lead to load shedding (blackout) or even system collapse

Frequency deviation is global control signal for participating generators and loads

Automatic generation control (AGC) : hierarchical control

- Primary (droop) control: stabilize frequency in ~30 secs
 - Uses governor to adjust valve position and control mechanical output of turbine
 - Control proportional to local frequency deviation
 - Decentralized



Frequency deviation is global control signal for participating generators and loads

Automatic generation control (AGC) : hierarchical control

- Secondary control: restore nominal frequency within a few mins
 - Adjust generator setpoints around dispatch values
 - Interconnected system: also restore scheduled tie-line flows between areas (need non-local info of tie-line flow deviations)
 - Each area is controlled centrally by an operator



Frequency deviation is global control signal for participating generators and loads

Automatic generation control (AGC) : hierarchical control

- Tertiary control: real-time optimal dispatch every 5-15 mins
 - Determine generator setpoints and schedule inter-area tie-line flows
 - Optimize across areas for economic efficiency
 - Restore reserve capacities of primary & secondary control so that they are available for contingency response



Frequency control Model

Primary and secondary control model

- Fix control interval *n*
- Fix random realization ξ of $\sigma(t)$

Assumptions (DC power flow)

- Lossless lines $y_{jk}^s = ib_{jk}$
- Fixed voltage magnitudes (voltage control operates at faster timescale)
- Small angle difference $\sin\left(\theta_{jk}\right) \approx \theta_{jk}$
- \implies Linearized dynamic model on
 - How real power control voltage angles & local frequencies (derivatives)

Frequency control Model

Linearized around operating point, defined by

$$u_j^0 + \sigma_j^0 = \sum_{k:j\sim k} P_{jk}^0$$



Primary frequency control Turbine-governor model

2nd order model with droop control

$$T_{gj}\dot{a}_j = -a_j(t) + u_j(t) - \frac{\Delta\omega_j(t)}{R_j}$$
$$T_{tj}\dot{p}_j^M = -p_j^M(t) + a_j(t)$$

where

- $a_i(t)$: valve position of turbine-governor
- $p_i^M(t)$: mechanical power output of turbine
- $u_i(t)$: generator setpoint (operating point u_i^0 is from tertiary control)
- $\Delta \omega_j(t) = \Delta \dot{\theta}_j(t)$: frequency deviation from operating-point frequency ω^0





Primary frequency control Turbine-governor model

Linearized around operating point

$$T_{gj}\Delta\dot{a}_{j} = -\Delta a_{j}(t) + \Delta u_{j}(t) - \frac{\Delta\omega_{j}(t)}{R_{j}}$$
$$T_{tj}\Delta\dot{p}_{j}^{M} = -\Delta p_{j}^{M}(t) + \Delta a_{j}(t)$$

incremental vars:

- $\Delta a_j(t) := a_j(t) a_j^0$: deviation of valve position of turbine-governor
- $\Delta p_j^M(t) := p_j^M(t) P_j^{M0}$: deviation of mechanical power output of turbine
- $\Delta u_j(t) := u_j(t) u_j^0$: adjustment to dispatched setpoint

Primary frequency control Turbine-governor model

Linearized around operating point

$$T_{gj}\Delta\dot{a}_{j} = -\Delta a_{j}(t) + \Delta u_{j}(t) - \frac{\Delta\omega_{j}(t)}{R_{j}}$$

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Primary frequency control Turbine-governor model

Linearized around operating point

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$$T_{tj} \Delta \dot{p}_{j}^{M} = -\Delta p_{j}^{M}(t) + \Delta a_{j}(t)$$
For primary control, $\Delta u_{j}(t) = \Delta u_{j}$ is constant
• $\Delta u_{j}(t)$ is adjusted by secondary control on a slower timescale
$$\Delta u_{j}(t) = \Delta u_{j} = \Delta u_{j}$$

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Primary frequency control Turbine-governor model

Linearized around operating point

$$T_{gj}\Delta\dot{a}_{j} = -\Delta a_{j}(t) + \Delta u_{j}(t) - \frac{\Delta\omega_{j}(t)}{R_{j}}$$
$$T_{tj}\Delta\dot{p}_{j}^{M} = -\Delta p_{j}^{M}(t) + \Delta a_{j}(t)$$

Equilibrium of turbine-governor (primary control):

$$\Delta \dot{a}_j(t) = \Delta \dot{p}_j^M = 0$$

Therefore

$$\Delta p_j^{M^*} = \Delta a_j^* = \Delta u_j - \frac{1}{R_i} \Delta \omega_j^*,$$

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Primary frequency control **Turbine-governor model**

Linearized around operating point

$$T_{gj} \Delta \dot{a}_{j} = -\Delta a_{j}(t) + \Delta u_{j}(t) - \frac{\Delta \omega_{j}(t)}{R_{j}}$$

$$T_{tj} \Delta \dot{p}_{j}^{M} = -\Delta p_{j}^{M}(t) + \Delta a_{j}(t)$$
Equilibrium of turbine-governor (primary control):
$$Au_{j} \xrightarrow{Au_{j}} \sqrt{\frac{1}{(t+sT_{j})(t+sT_{t})}} \xrightarrow{Ap_{j}^{M}}$$
Increased as $\Delta \omega_{j}^{*} \neq 0$

$$Frequency deviation \Delta \omega_{j}^{*} \neq 0$$

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- Incremental mechanical power $\Delta p_{i}^{M^{st}}$ depends on $\Delta \omega_{i}^{st}$

$$\Delta \dot{\theta}_{j} = \Delta \omega_{j}(t)$$

$$M_{j} \Delta \dot{\omega}_{j} + D_{j} \Delta \omega_{j}(t) = \Delta p_{j}^{M}(t) + \Delta \sigma_{j}(t) - \sum_{k:j \sim k} \Delta P_{jk}(t)$$

where

- $\Delta \theta_j(t) := \theta_j(t) \theta_j^0$: incremental angle relative to rotating frame of ω^0
- $\Delta \sigma_i(t)$: deviation of uncontrollable injection from its forecast σ_i^0
- $\Delta P_{jk}(t) := P_{jk}(t) P_{jk}^0$: line flow deviation



$$\Delta \dot{\theta}_{j} = \Delta \omega_{j}(t)$$

$$M_{j} \Delta \dot{\omega}_{j} + D_{j} \Delta \omega_{j}(t) = \Delta p_{j}^{M}(t) + \Delta \sigma_{j}(t) - \sum_{k:j \sim k} \Delta P_{jk}(t)$$

where

- M_i : inertia constant of synchronous machine
- D_i : damping and frequency-sensitive load



Model for instantaneous line flow

$$P_{jk}(t) = |V_j| |V_k| \left(-b_{jk}\right) \sin\left(\theta_j(t) - \theta_k(t)\right)$$

Model for instantaneous line flow

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Linear approximation

$$P_{jk}(t) = |V_j| |V_k| \left(-b_{jk}\right) \sin\left(\theta_j^0 - \theta_k^0\right) + T_{jk} \left(\Delta \theta_j(t) - \Delta \theta_k(t)\right)$$

$$\underbrace{P_{jk}^0}_{P_{jk}^0}$$

Model for instantaneous line flow

$$P_{jk}(t) = |V_j| |V_k| \left(-b_{jk}\right) \sin\left(\theta_j(t) - \theta_k(t)\right)$$

Linear approximation

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$$\underbrace{P_{jk}^0}_{P_{jk}^0}$$

Linearized model

$$\Delta P_{jk}(t) = T_{jk} \left(\Delta \theta_j(t) - \Delta \theta_k(t) \right)$$

where $T_{jk} := |V_j| |V_k| \left(-b_{jk} \right) \cos \left(\theta_j^0 - \theta_k^0 \right)$



Primary frequency control Turbine-governor-generator model

$$T_{gj}\Delta\dot{a}_{j} = -\Delta a_{j}(t) + \Delta u_{j}(t) - \frac{\Delta\omega_{j}(t)}{R_{j}}$$

$$T_{tj}\Delta\dot{p}_{j}^{M} = -\Delta p_{j}^{M}(t) + \Delta a_{j}(t)$$

$$M_{j}\Delta\dot{\omega}_{j} + D_{j}\Delta\omega_{j}(t) = \Delta p_{j}^{M}(t) + \Delta\sigma_{j}(t) - \sum_{k:j\sim k}\Delta P_{jk}(t)$$

$$\Delta P_{jk}(t) = T_{jk}\left(\Delta\theta_{j}(t) - \Delta\theta_{k}(t)\right)$$

$$\Delta\dot{\theta}_{j} = \Delta\omega_{j}(t)$$

Primary frequency control

Turbine-governor-generator model



Primary frequency control Turbine-governor-generator model

$$T_{gj} \Delta \dot{a}_{j} = -\Delta a_{j}(t) + \Delta u_{j}(t) - \frac{\Delta \omega_{j}(t)}{R_{j}}$$

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$$\Delta P_{jk}(t) = T_{jk} \left(\Delta \theta_{j}(t) - \Delta \theta_{k}(t) \right)$$

$$\Delta \dot{\theta}_{j} = \Delta \omega_{j}(t)$$

Equilibrium of primary control: $\Delta \dot{\omega}_j = \Delta \dot{a}_j = \Delta \dot{p}_j^M = 0$ (does not require $\Delta \dot{\theta} = 0$) Steven Low EE/CS/EST 135 Caltech

Bus-by-line incidence matrix C:

$$C_{jl} := \begin{cases} 1 & \text{if } l = j \to k \text{ for some bus } k \\ -1 & \text{if } l = i \to j \text{ for some bus } i \\ 0 & \text{otherwise} \end{cases}$$

Stiffness matrix: $T := \text{diag}(T_{jk}, (j, k) \in E)$ Laplacian matrix: $L := CTC^T$ and its pseudo-inverse L^{\dagger}

Theorem

Let $x^* := (\Delta \omega^*, \Delta P^*, \Delta \theta^*, \Delta a^*, \Delta p^{M^*})$ be an equilibrium driven by step change $\Delta \sigma$ and constant setpoint Δu

Theorem

Let $x^* := (\Delta \omega^*, \Delta P^*, \Delta \theta^*, \Delta a^*, \Delta p^{M^*})$ be an equilibrium driven by step change $\Delta \sigma$ and constant setpoint Δu

1. Local frequency deviations converge to

$$\Delta \omega_{j}^{*} = \Delta \omega^{*} := \frac{\sum_{k} \left(\Delta u_{k} + \Delta \sigma_{k} \right)}{\sum_{k} \left(D_{k} + 1/R_{k} \right)}$$

Theorem

Let $x^* := (\Delta \omega^*, \Delta P^*, \Delta \theta^*, \Delta a^*, \Delta p^{M^*})$ be an equilibrium driven by step change $\Delta \sigma$ and constant setpoint Δu

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2. Line flow deviations converge to

$$\begin{split} \Delta P^* &= TC^T L^\dagger \left(\Delta u \ + \ \Delta \sigma \ - \ \Delta \omega^* d \right) \\ \text{where } d \ := \ (D_j + 1/R_j, j \in \overline{N}) \end{split}$$

Theorem

Let $x^* := (\Delta \omega^*, \Delta P^*, \Delta \theta^*, \Delta a^*, \Delta p^{M^*})$ be an equilibrium driven by step change $\Delta \sigma$ and constant setpoint Δu

1. Local frequency deviations converge to

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2. Line flow deviations converge to

$$\begin{split} \Delta P^* &= TC^T L^\dagger \left(\Delta u \ + \ \Delta \sigma \ - \ \Delta \omega^* d \right) \\ \text{where } d \ := \ (D_j + 1/R_j, j \in \overline{N}) \end{split}$$

Secondary control: • Adjusting Δu to drive $\Delta \omega_j^*$ and ΔP_{jk}^* to 0

Primary frequency control Example: interconnected system

Model

- N + 1 areas each modeled as a bus
- $\Delta u_j = 0$ for all j
- Step change: at time 0, $\sigma_i(t)$ changes from 0 to a constant value $\Delta\sigma_i$
- Suppose $\Delta \sigma_i$ are iid random variables with mean $\Delta \bar{\sigma}_i$ and variance v_i^2

Compare the mean & variance of equilibrium frequency deviation $\Delta \omega_i^*$:

- Case 1: the areas (buses) are not connected and operate independently.
- Case 2: the areas (buses) are connected into a network

Primary frequency control Example: interconnected system

Case 1: independent operation

$$\Delta \omega_{j}^{*} = \frac{\Delta \sigma_{j}}{d_{j}} \quad \text{where } d_{j} := D_{j} + 1/R_{j}$$

with $E\Delta \omega_{j}^{*} = \frac{\Delta \bar{\sigma}_{j}}{d_{j}}, \quad \text{var} \left(\Delta \omega_{j}^{*}\right) = \frac{v_{j}^{2}}{d_{j}^{2}}$

Case 2: interconnected system

$$\begin{split} \Delta \omega^* &= \frac{\sum_j \Delta \sigma_j}{\sum_j d_j} = \frac{1}{N+1} \sum_j \frac{\Delta \sigma_j}{\hat{d}} \qquad \text{where } \hat{d}_j := \frac{1}{N+1} \sum_j d_j \\ \text{with} & E \Delta \omega^* = \frac{\Delta \hat{\sigma}}{\hat{d}}, \quad \text{var}(\Delta \omega^*) = \frac{1}{N+1} \frac{\hat{v}^2}{\hat{d}^2} \qquad \text{where } \Delta \hat{\sigma}, \, \hat{v}^2 \text{ are avgerages} \end{split}$$

Frequency control Model

Linearized around operating point, defined by

$$u_j^0 + \sigma_j^0 = \sum_{k:j \sim k} P_{jk}^0$$

Incremental variables (full list)

- $\Delta u_j(t) := u_j(t) u_j^0$: adjustment to dispatched setpoint
- $\Delta \theta_j(t) := \theta_j(t) \theta_j^0$: incremental angle relative to rotating frame of ω^0
- $\Delta \omega_j(t) = \Delta \dot{\theta}_j(t)$: frequency deviation from operating-point frequency ω^0
- $\Delta P_{jk}(t) := P_{jk}(t) P_{jk}^0$: line flow deviation
- $\Delta p_j^M(t) := p_j^M(t) P_j^{M0}$: deviation of mechanical power output of turbine
- $\Delta a_j(t) := a_j(t) a_j^0$: deviation of valve position of turbine-governor

Outline

- 1. Overview
- 2. Unit commitment
- 3. Optimal dispatch

4. Frequency control

- Model and assumptions
- Primary frequency control
- Secondary frequency control
- 5. System security

Secondary frequency control Objectives

- 1. Restore frequency to nominal value
 - Drive $\Delta \omega^* = 0$
- 2. Restore tie-line flows to scheduled values (scheduled by tertiary control)
 - Drive $\Delta P^* = 0$ (each bus represents a control area)

Secondary frequency control Objectives

At equilibrium of primary control :

$$\Delta \omega_{j}^{*} = \Delta \omega^{*} := \frac{\sum_{k} (\Delta u_{k} + \Delta \sigma_{k})}{\sum_{k} (D_{k} + 1/R_{k})}$$
$$\Delta P^{*} = TC^{T}L^{\dagger} (\Delta u + \Delta \sigma - \Delta \omega^{*}d)$$

Therefore, need to adjust setpoints $\Delta u(t)$ • $\Delta \omega_j^* = 0$ if $\sum_k (\Delta u_k + \Delta \sigma_k) = 0$ • $\Delta P_{jk}^* = 0$ if $\Delta u_j + \Delta \sigma_j = 0$

Secondary frequency control

Area control error (ACE)

$$ACE_{j}(t) := \sum_{k:j\sim k} \Delta P_{jk}(t) + \beta_{j} \Delta \omega_{j}(t)$$

Setpoint adjustment

$$\Delta \dot{u}_{j} = -\gamma_{j} \left(\sum_{k:j \sim k} \Delta P_{jk}(t) + \beta_{j} \Delta \omega_{j}(t) \right)$$

Implementation

- Real-time measurements of $P_{ik}(t)$ with neighboring areas k are sent to system operator
- System operator centrally computes $\Delta \dot{u}_j$ and dispatch setpoint adjustments $\alpha_{ji}\Delta u_j(t)$ to participating generators i in areal j ($\alpha_{ji} \ge 0$ with $\sum \alpha_{ji} = 1$ are called participation factors)

Secondary frequency control Overall (primary & secondary) model

$$T_{g}\Delta\dot{a} = -\Delta a(t) + \Delta u(t) - R^{-1}\Delta\omega(t)$$

$$T_{t}\Delta\dot{p}^{M} = -\Delta p^{M}(t) + \Delta a(t)$$

$$M\Delta\dot{\omega} + D\Delta\omega(t) = \Delta p^{M}(t) + \Delta\sigma(t) - C\Delta P(t)$$

$$\Delta P(t) = TC^{T}\Delta\theta(t)$$

$$\Delta\dot{\theta} = \Delta\omega(t)$$

$$\Delta\dot{u} = -\Gamma \left(C\Delta P(t) + B\Delta\omega(t)\right)$$
generator

Equilibrium of secondary control: $\Delta \dot{u} = \Delta \dot{\omega} = \Delta \dot{a} = \Delta \dot{p}^M = 0$ (does not req $\Delta \dot{\theta} = 0$)

Secondary frequency control

Overall (primary & secondary) model



Secondary frequency control Equilibrium

Theorem

Let $x^* := (\Delta u^*, \Delta \omega^*, \Delta P^*, \Delta \theta^*, \Delta a^*, \Delta p^{M^*})$ be an equilibrium driven by step change $\Delta \sigma$

1. Frequencies are restored to ω^0 : $\Delta \omega^* = 0$

Secondary frequency control Equilibrium

Theorem

Let $x^* := (\Delta u^*, \Delta \omega^*, \Delta P^*, \Delta \theta^*, \Delta a^*, \Delta p^{M^*})$ be an equilibrium driven by step change $\Delta \sigma$

- 1. Frequencies are restored to ω^0 : $\Delta \omega^* = 0$
- 2. Line flow are restored to P^0 : $\Delta P^* = 0$

Secondary frequency control Equilibrium

Theorem

Let $x^* := (\Delta u^*, \Delta \omega^*, \Delta P^*, \Delta \theta^*, \Delta a^*, \Delta p^{M^*})$ be an equilibrium driven by step change $\Delta \sigma$

- 1. Frequencies are restored to ω^0 : $\Delta \omega^* = 0$
- 2. Line flow are restored to P^0 : $\Delta P^* = 0$
- 3. Disturbances are compensated for locally at each bus (i.e., in each area) : $\Delta u_j^* + \Delta \sigma_{\!j} = 0$

Outline

- 1. Overview
- 2. Unit commitment
- 3. Optimal dispatch
- 4. Frequency control
- 5. System security

System security

- System security refers to ability to withstand contingency events
- A contingency event is an outage of a generator, transmission line, or transformer
- Contingency events are rare, but can be catastrophic
- NERC's (North America Electricity Reliability Council) N-1 rule the outage of a single piece of equipment should not result in violation of voltage or line limits

System security

Secure operation

- Analyze credible contingencies that may lead to voltage or line limit violations
- Account for these contingencies in optimal commitment and dispatch schedules (security constrained UC/ED)
- Monitor system state in real time and take corrective actions when contingency arises

Optimal dispatch

Recall: OPF without security constraints (base case):

$$\min_{\substack{(u_0, x_0) \\ \text{s.t.}}} c_0(u_0, x_0)$$

$$f_0(u_0, x_0) = 0, g_0(u_0, x_0) \le 0$$

where

- u_0 : dispatch in base case
- *x*₀ : network state in base case
- $f_0(u_0, x_0)$: power flow equations, etc.
- $g_0(u_0, x_0)$: operational constraints

Security constrained OPF Preventive approach

Basic idea

- Augment optimal dispatch (OPF) with additional constraints ...
- ... so that the (new) network state under optimal dispatch *u*^{opt} will satisfy operational constraints after contingency events
- Dispatch remains unchanged until next update period, even if a contingency occurs in the middle of control interval

Security constrained OPF Preventive approach

Security constrained OPF (SCOPF)

$$\begin{array}{ll} \min_{\substack{(u_0, x_0, \ \tilde{x}_k, \ k \ge 1)}} & c_0\left(u_0, x_0\right) \\ \text{s.t.} & f_0\left(u_0, x_0\right) \ = \ 0, \ g_0\left(u_0, x_0\right) \ \le \ 0 \ \text{ base case constraints} \\ & \tilde{f}_k\left(u_0, \tilde{x}_k\right) \ = \ 0, \ \ \tilde{g}_k\left(u_0, \tilde{x}_k\right) \ \le \ 0 \ \text{ constraints after cont. } k \end{array}$$

where

- \tilde{x}_k : new state under same dispatch u_0 after contingency k
- $\tilde{f}_0(u_0, \tilde{x}_0)$: power flow equations for post-contingency network
- $\tilde{g}_0(u_0, \tilde{x}_0)$: (more relaxed) emergency operational constraints after contingency k

Security constrained OPF Corrective approach

Basic idea

- Compute optimal dispatch not only for base case, but also for each contingency k
- System operator can dispatch a response immediately after contingency without waiting till next dispatch period
Security constrained OPF Corrective approach

Security constrained OPF (SCOPF)

$$\begin{array}{ll} \min_{(u_k, x_k, \ k \ge 0)} & \sum_{k \ge 0} w_k c_k \left(u_k, x_k \right) \\ \text{s.t.} & f_k \left(u_k, x_k \right) \ = \ 0, \ g_k \left(u_k, x_k \right) \ \le \ 0, \ \ k \ge 0 \\ & \|u_k - u_0\| \ \le \ \rho_k, \ \ k \ge 1 \end{array} \quad \text{ramp rate limits} \end{array}$$

where

- (u_k, x_k) : dispatch & state in base case k = 0 and after contingency $k \ge 1$
- (f_k, g_k) : power flow equations & operational constraints for $k \ge 0$
- $||u_k u_0||$: ramp rate limits

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Conclusion

Central challenge: balance supply & demand second-by-second

- While satisfying operational constraints, e.g. injection/voltage/line limits
- Unlike usual commodities, electricity cannot (yet) be stored in large quantity

This is achieved through a complex set of mechanisms that operate in concert across multiple timescales

- Slow timescale mechanisms (minutes and up) can be formulated as OPF problems
- Fast timescales (seconds to minutes) can be formulated as feedback control problems

Part III of text: OPF

• Mathematical formulations, computational properties, convex relaxations, stochastic optimization

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